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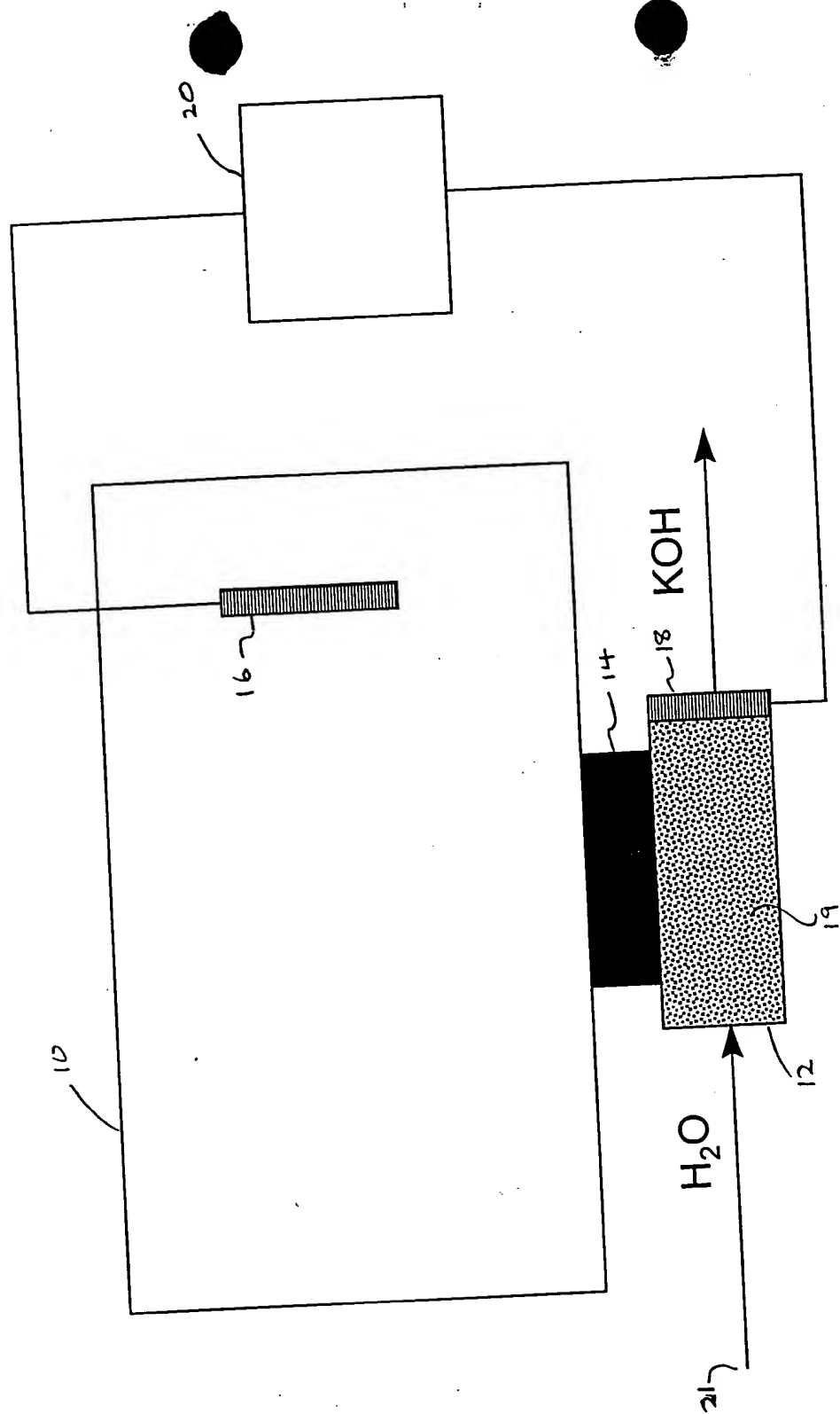


Figure 1.

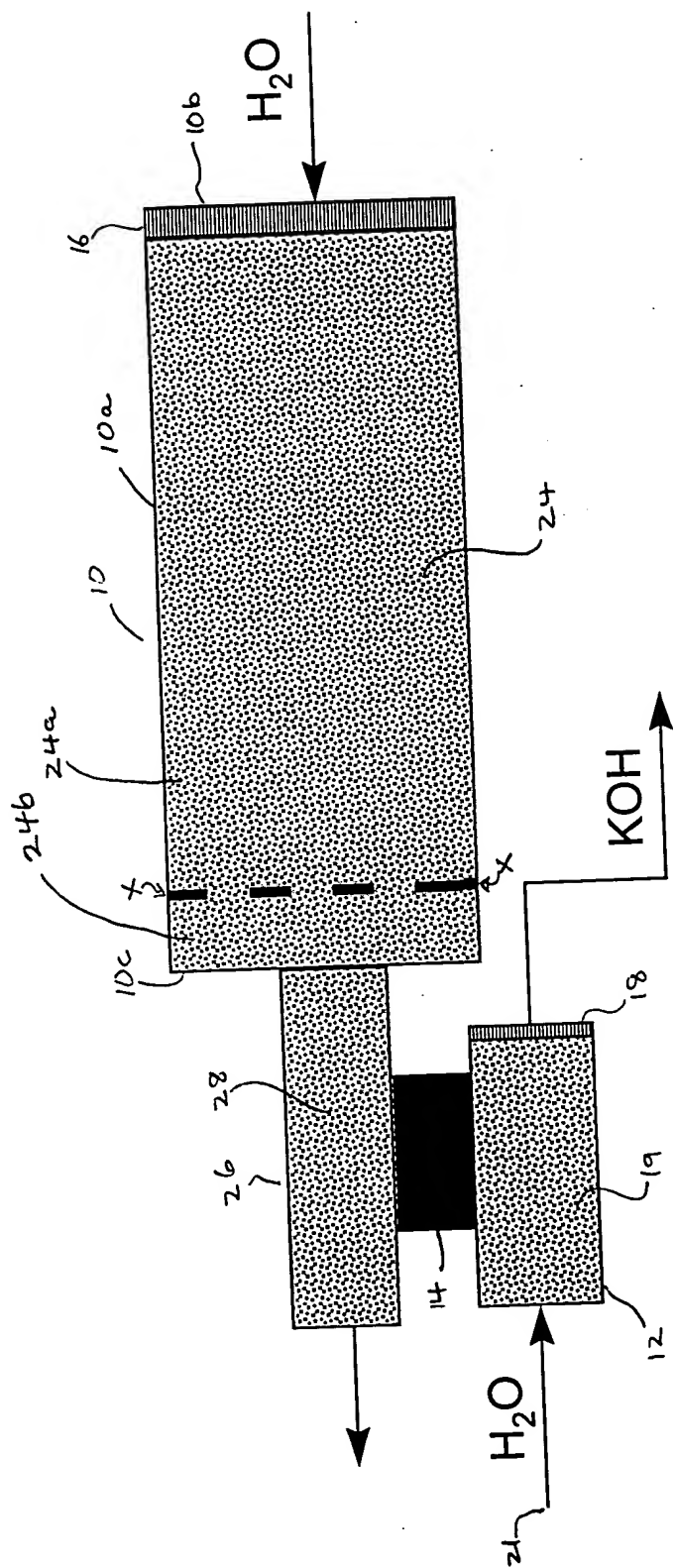


Figure 2.

FIG. 3 is a schematic diagram of a system for the production of hydrogen gas. The system includes a water supply (12) which feeds into a water electrolysis cell (14). The electrolysis cell is connected to a power source (16) via a circuit (10). The electrolysis cell produces hydrogen gas (H₂) which is collected in a gas collector (18). The gas collector is connected to a gas outlet (20) which leads to a gas storage tank (19). The gas storage tank is connected to a gas supply line (21) which feeds into a gas engine (22). The gas engine is connected to a power generator (24) which produces electricity (26). The electricity is fed back into the power source (16) via a circuit (10).

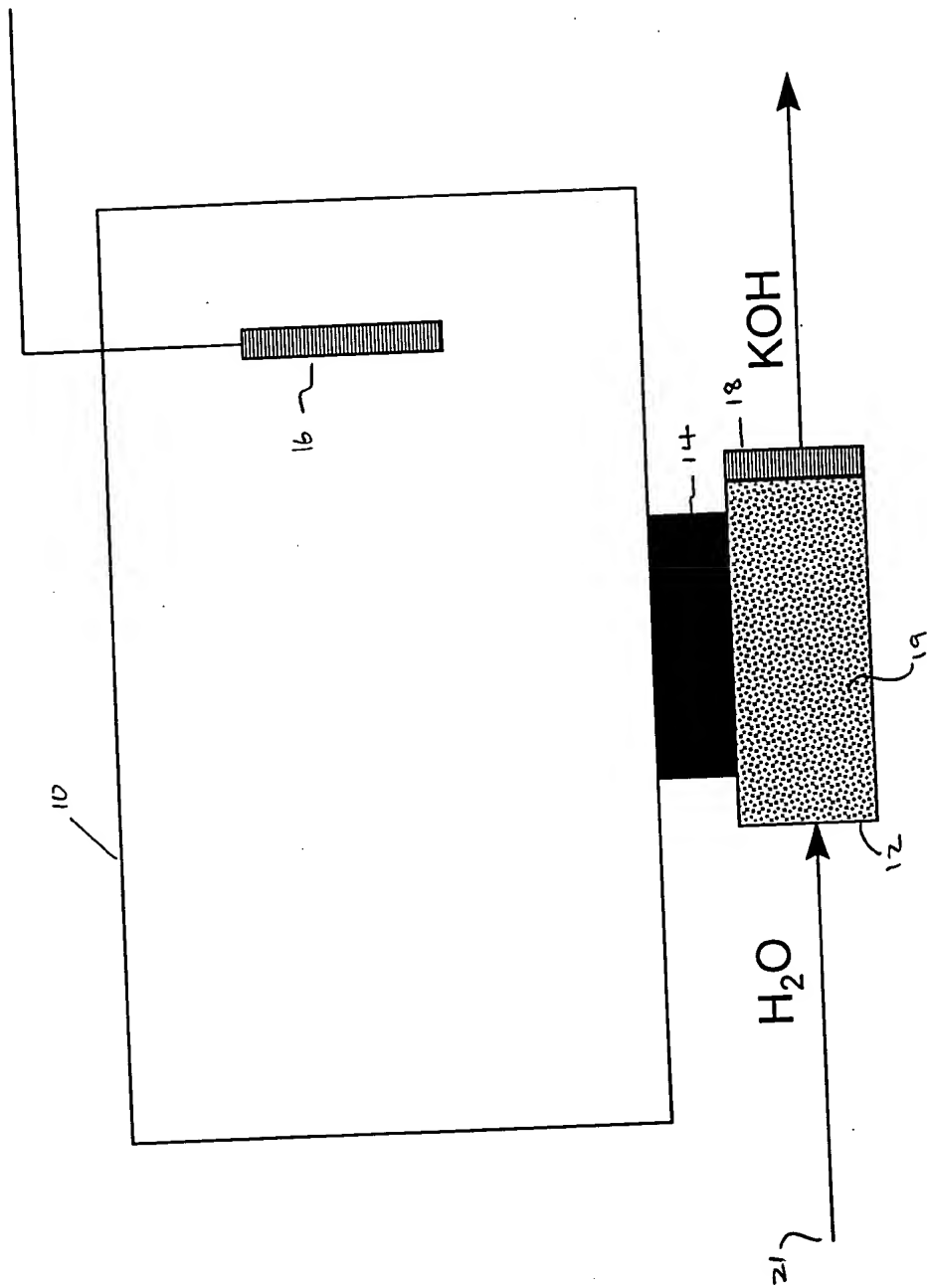


Figure 3.

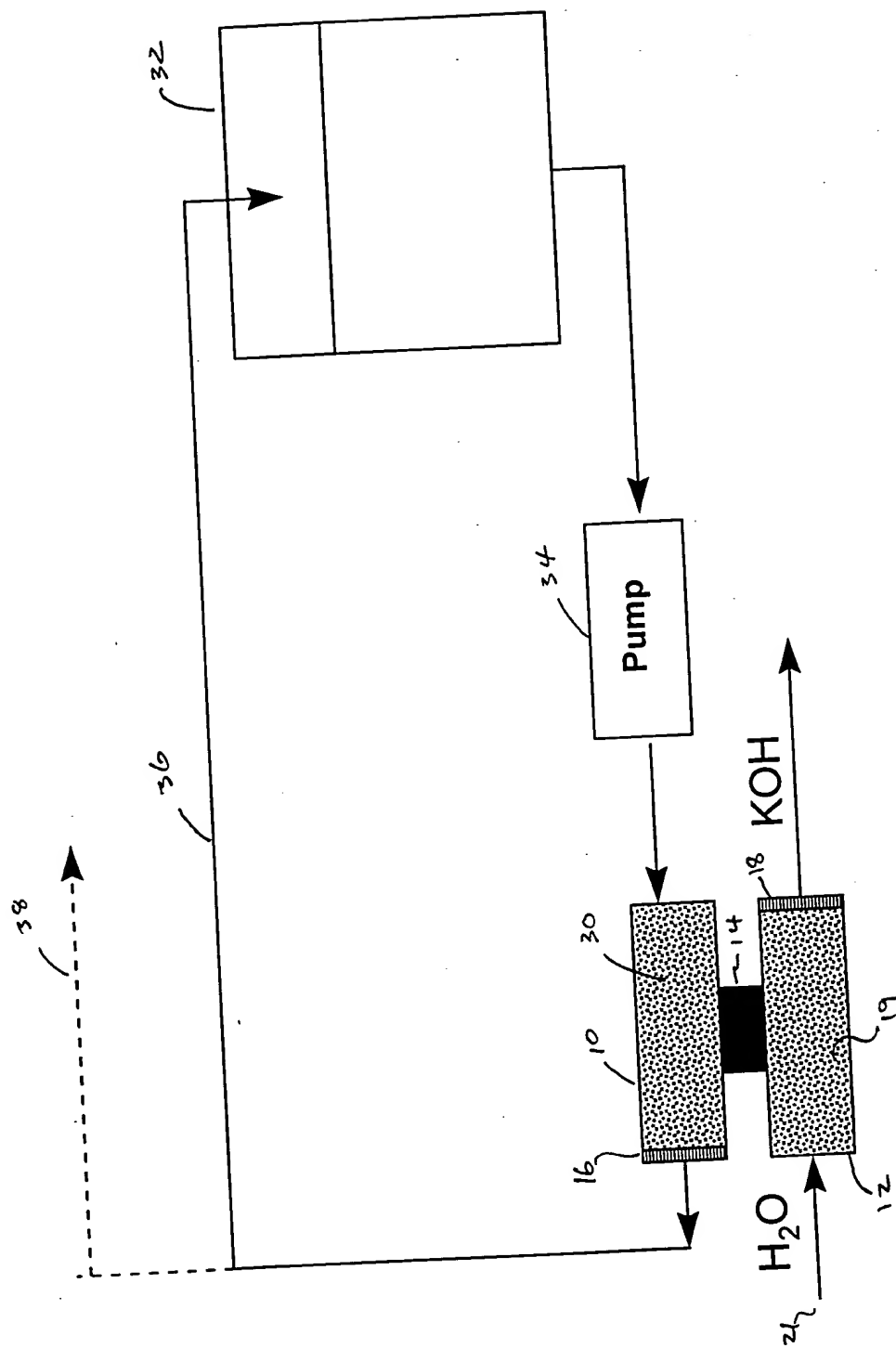


Figure 4.

The diagram illustrates a three-stage electrochemical cell, labeled 10, designed for hydrogen production. The cell consists of three vertical reaction chambers, 12a, 12b, and 12c, arranged in series. Each chamber contains a porous electrode 19 and a top layer 18 (18a, 18b, 18c). The chambers are separated by vertical dividers 14a, 14b, and 14c. Arrows indicate the flow of reactants: H_2O enters from the bottom left, and KOH enters from the top right. A horizontal line 16 is connected to the top of the first chamber 12a. The entire assembly is enclosed in a rectangular frame 10.

Figure 5.

any other suitable means for the purpose of the invention.

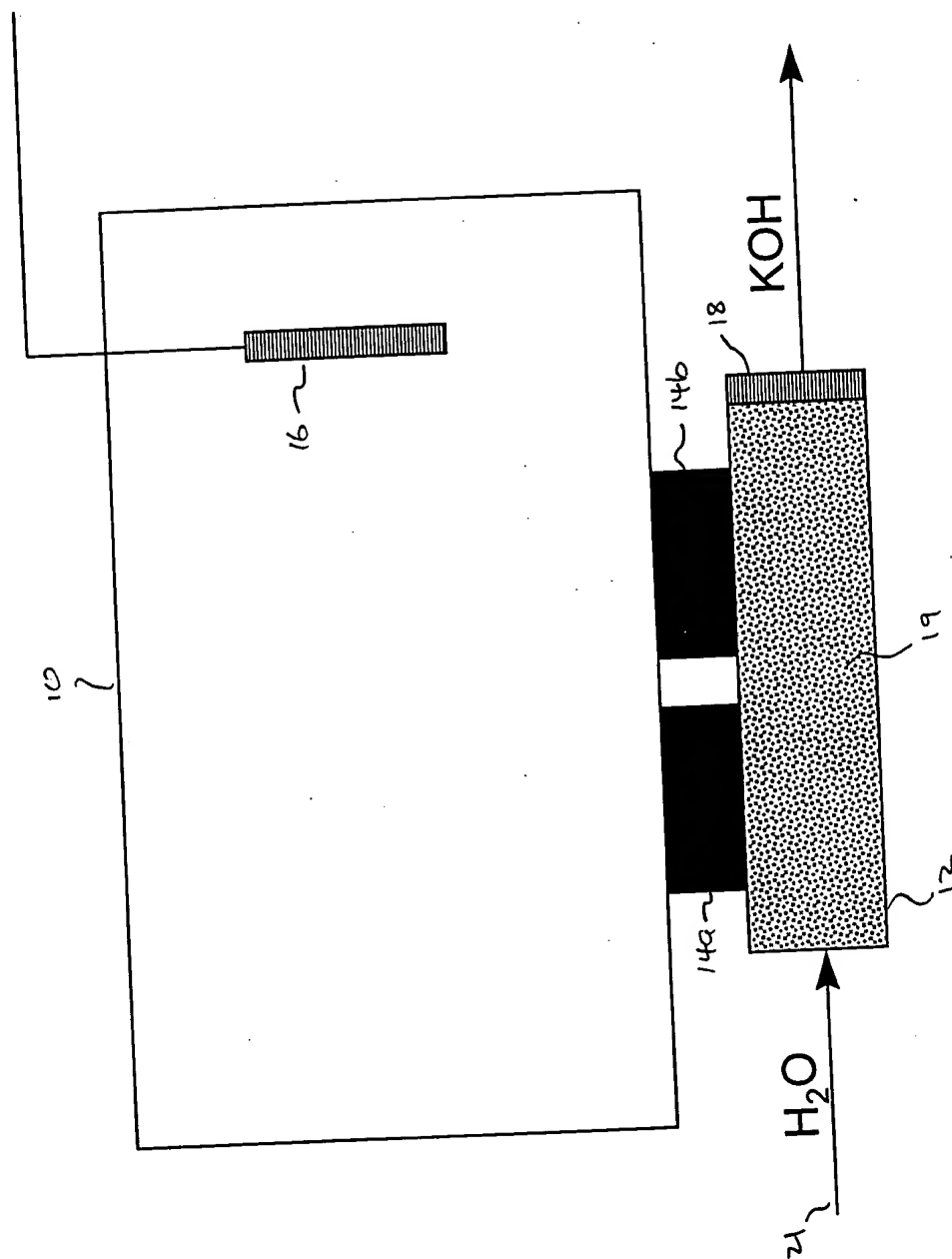


Figure 6.

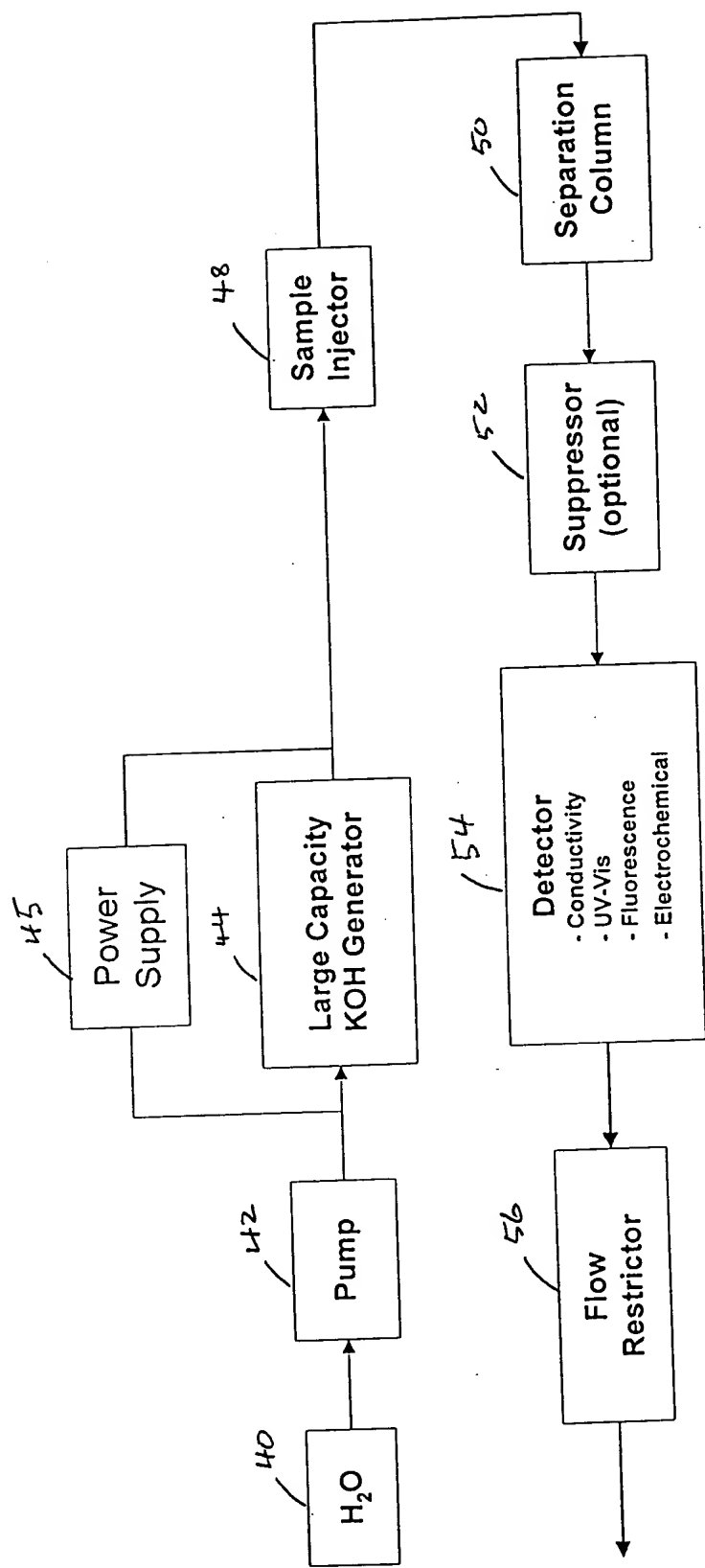


Figure 7.

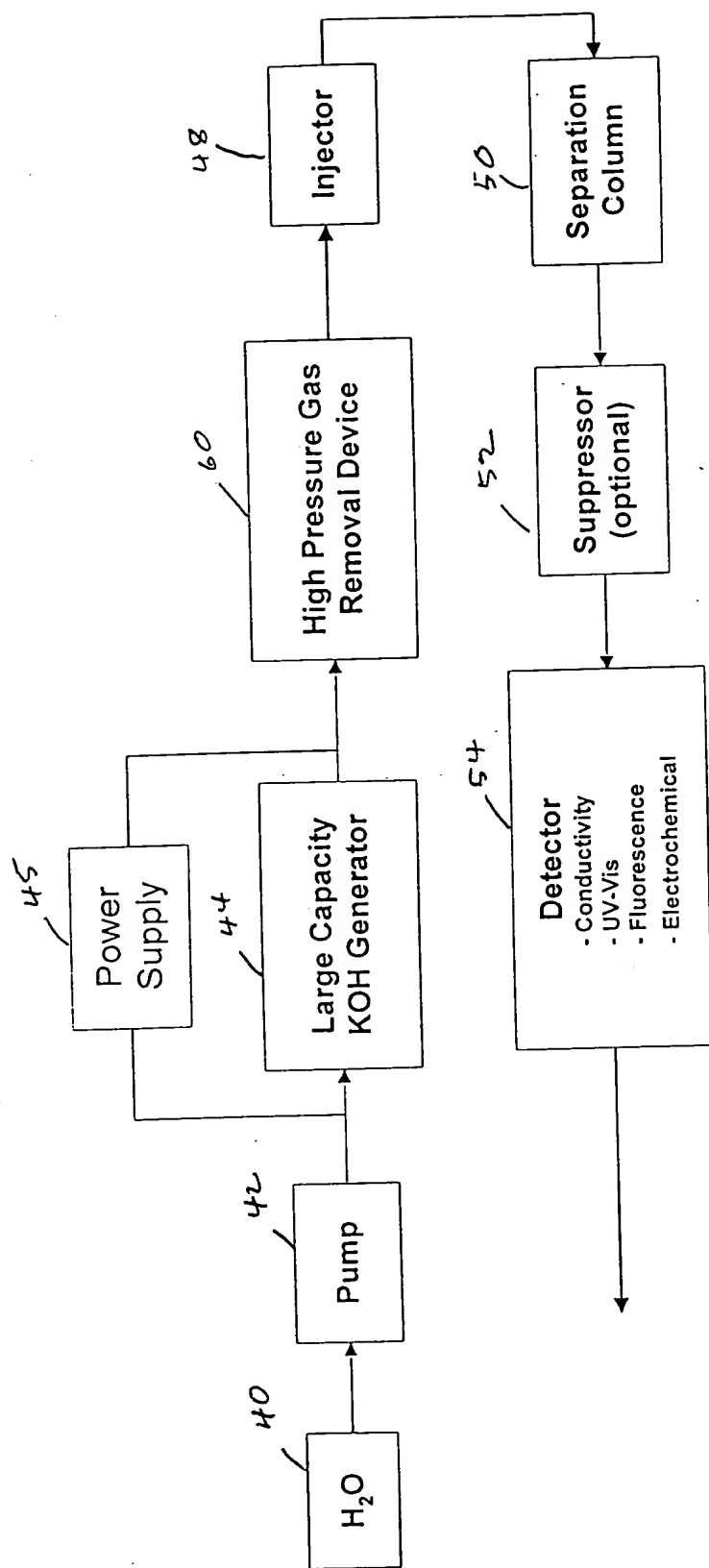


Figure 8.

Figure 9 is a schematic diagram of a chemical process. The diagram shows a horizontal rectangular vessel with an internal partition. On the left side, an inlet stream labeled $\text{KOH} + \text{H}_2$ enters through a line labeled 62. On the right side, an outlet stream labeled KOH exits through a line labeled 64. A third stream, labeled 67, exits from the top of the vessel. The vessel is divided into two sections by a vertical partition. The left section is labeled 66 and the right section is labeled 64.

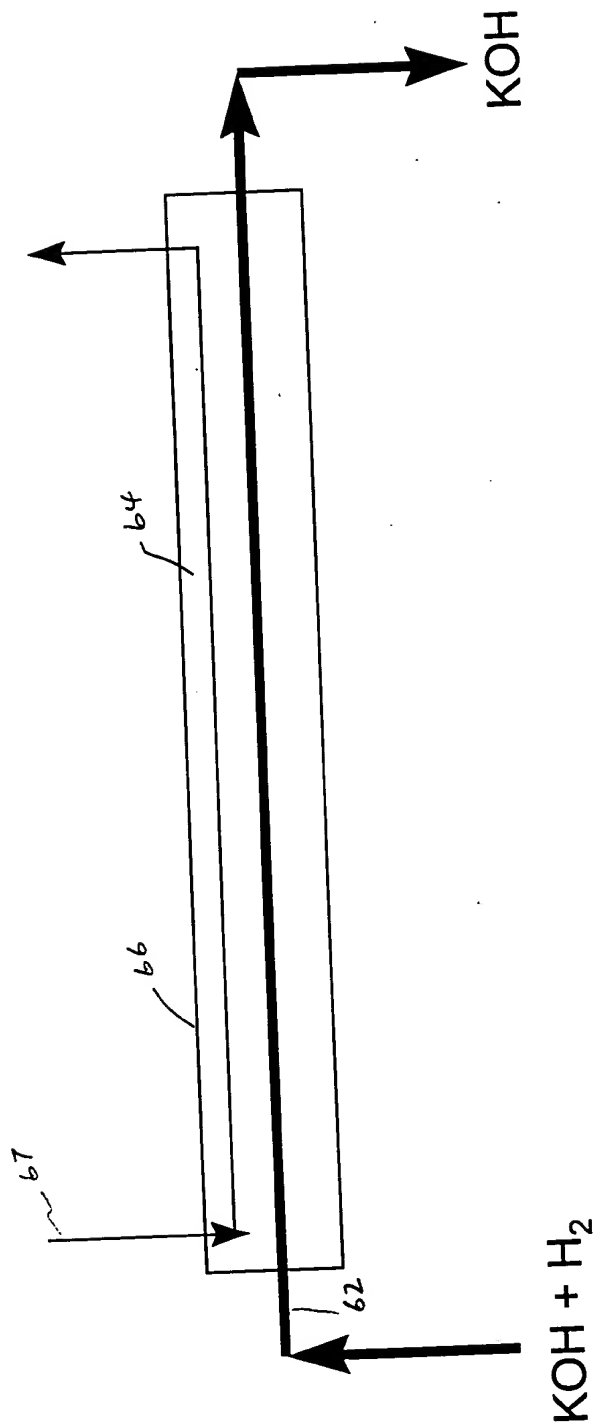


Figure 9.

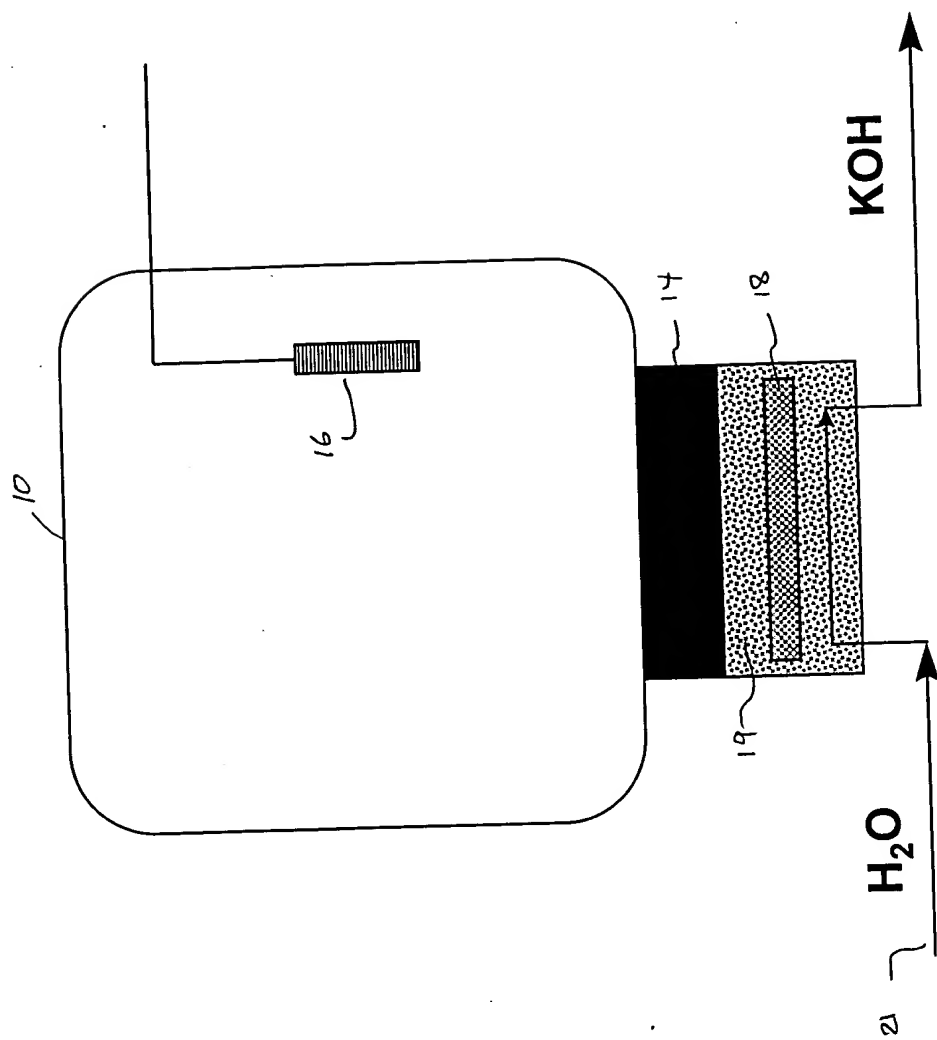


Figure 10.

FIG. 11 is a schematic diagram of a fuel cell system.

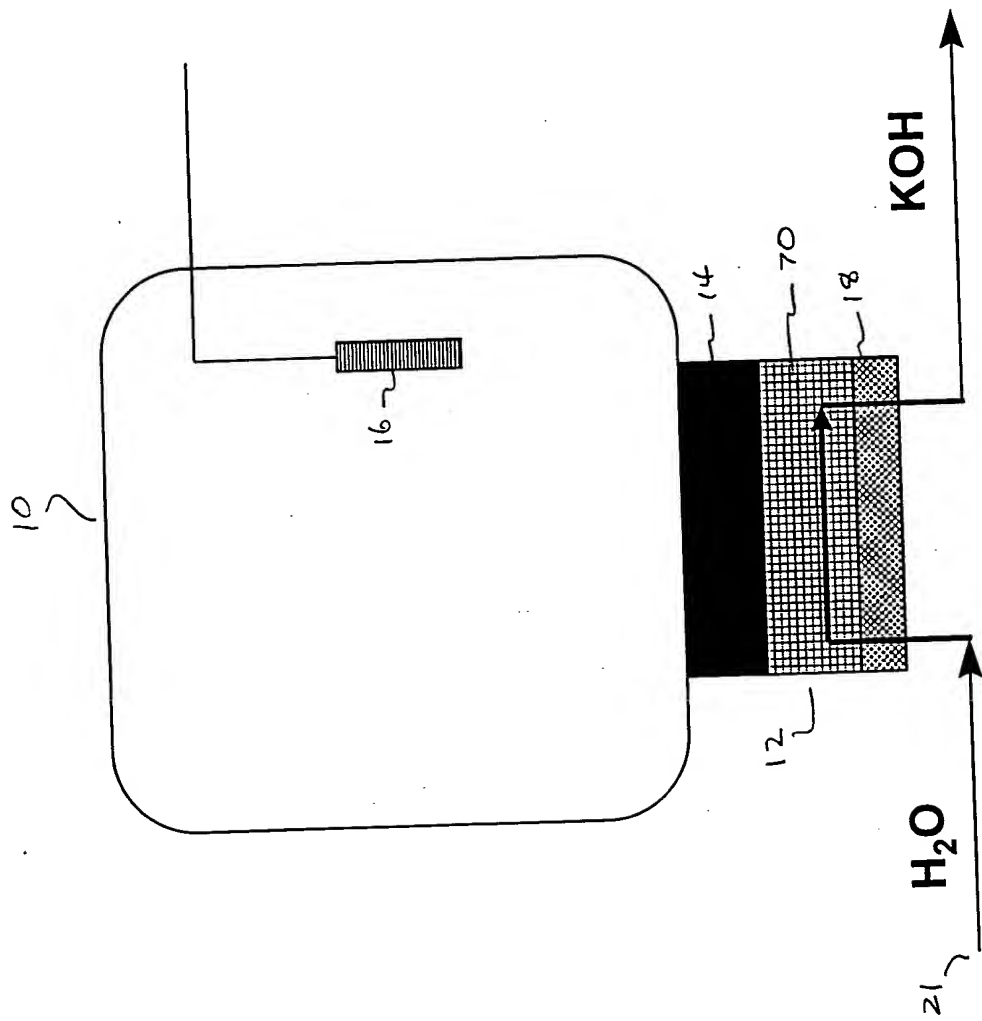


Figure 11.

any other suitable material for the purpose of the present invention.

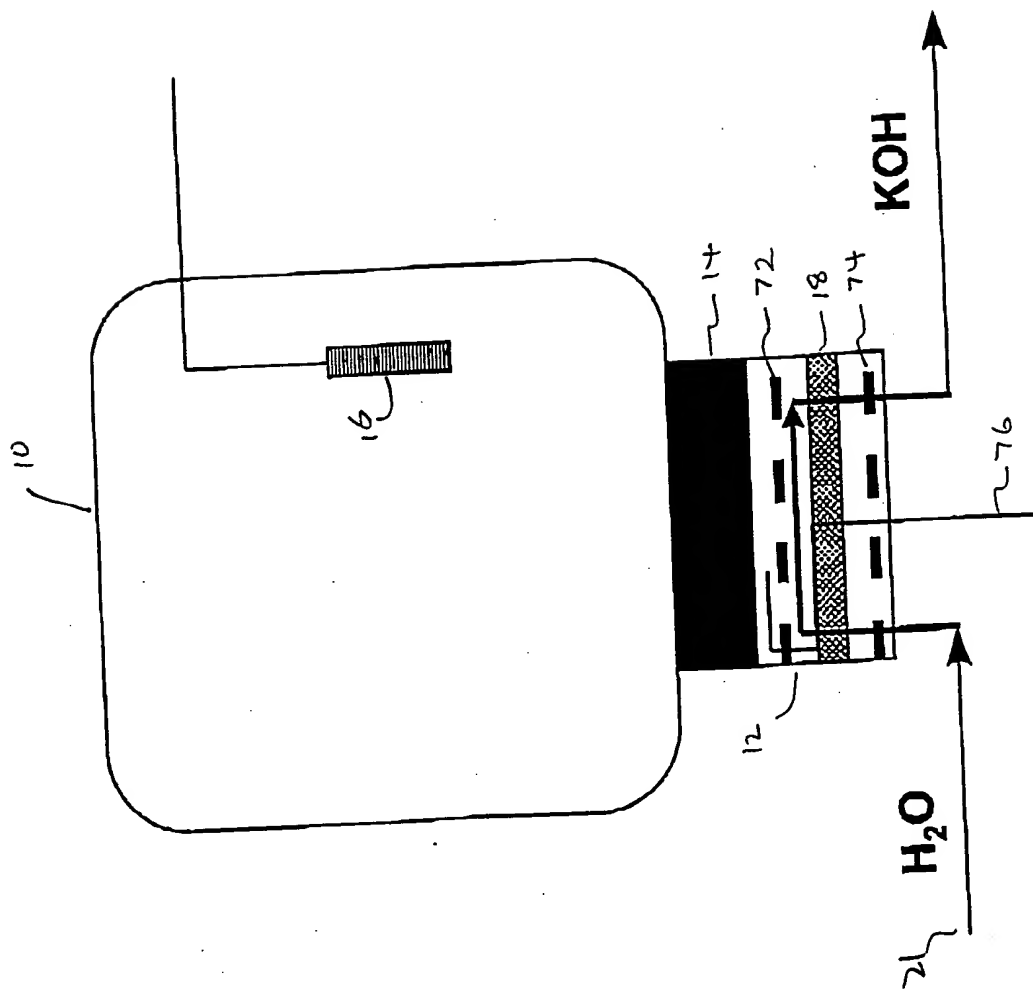


Figure 12.

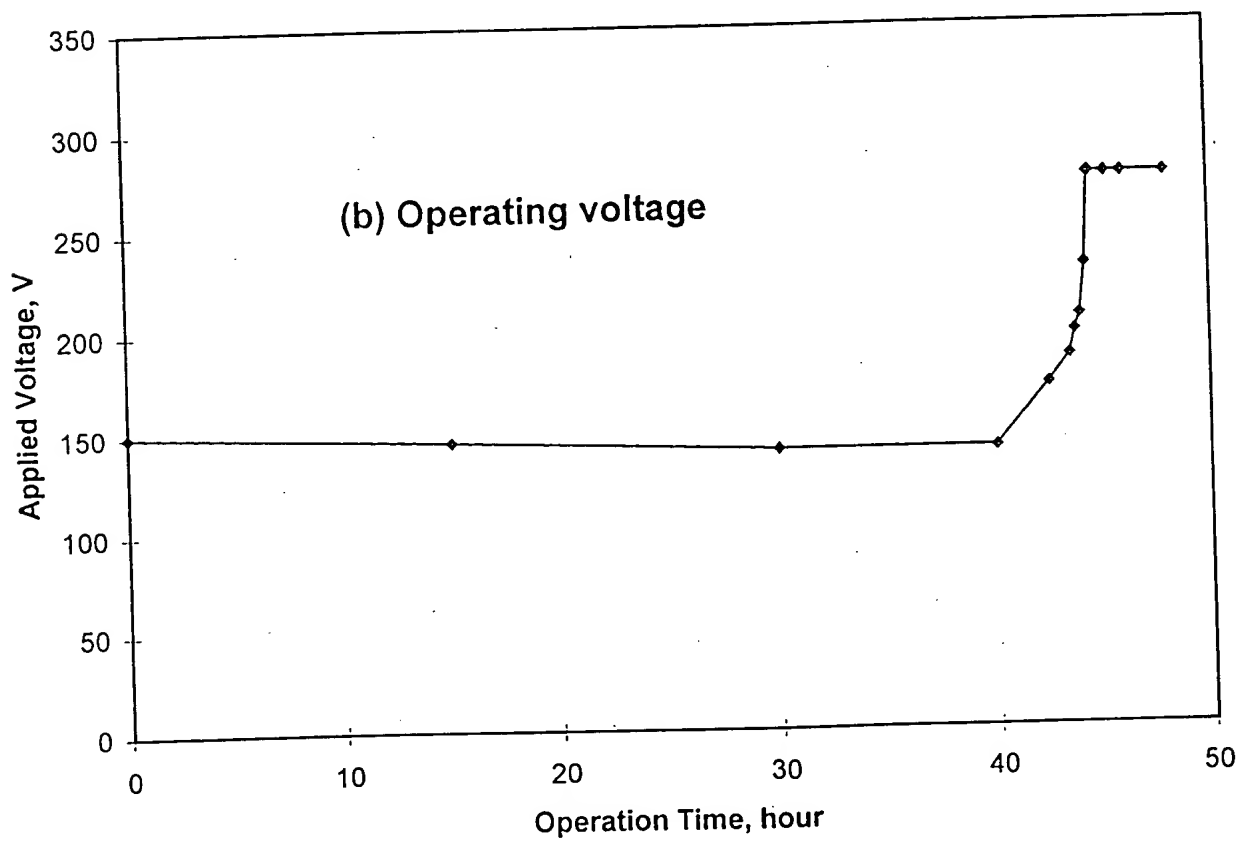
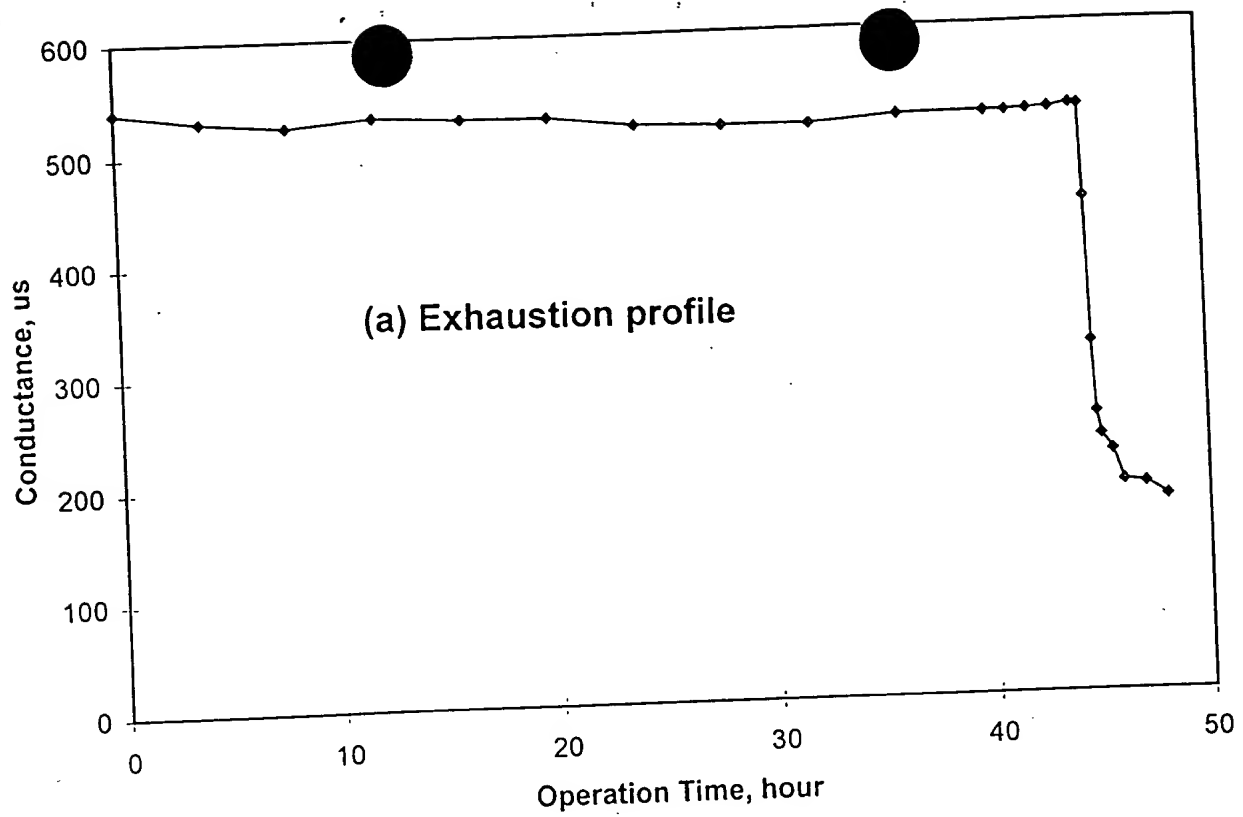


Figure 13.

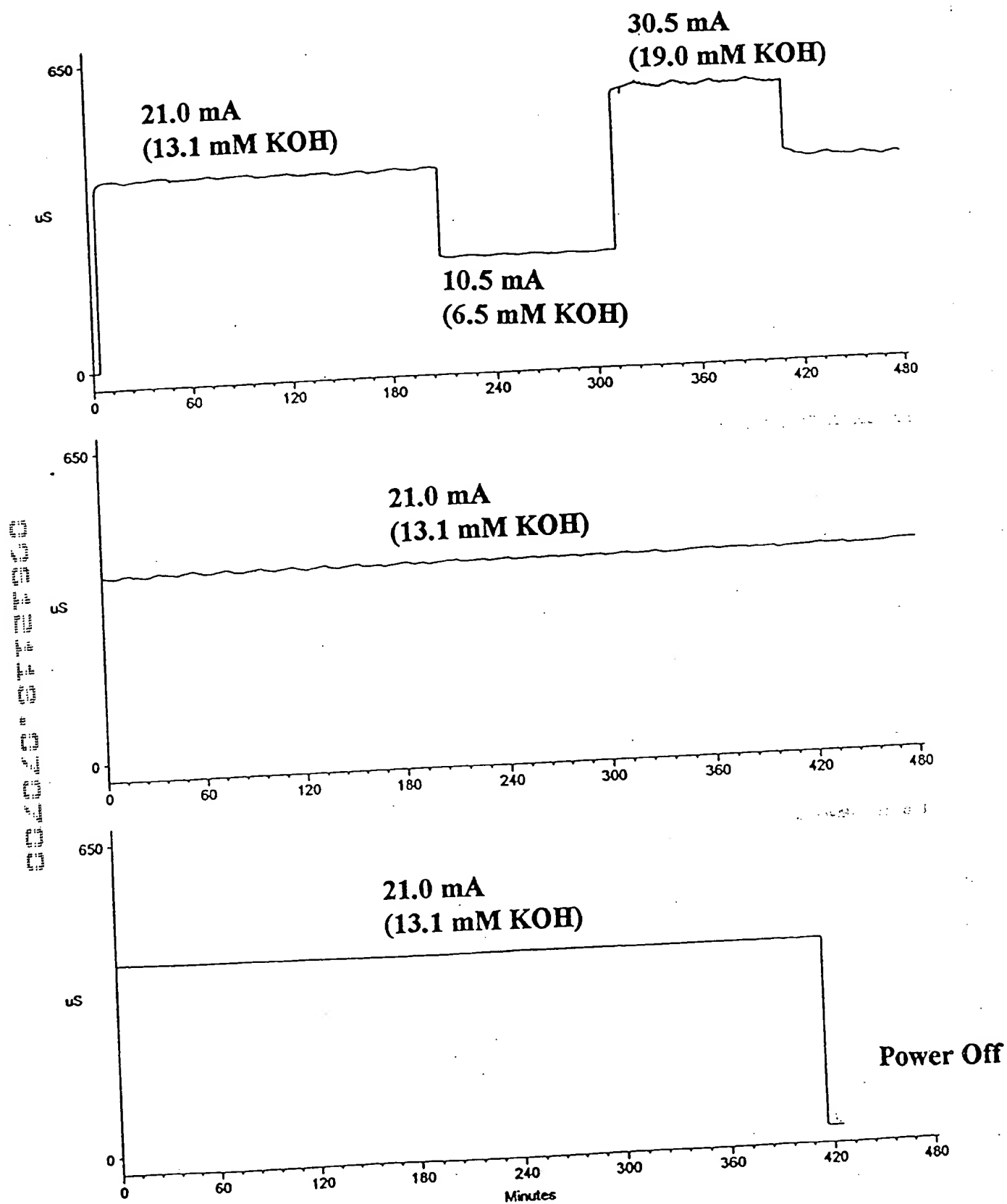


Figure 14.

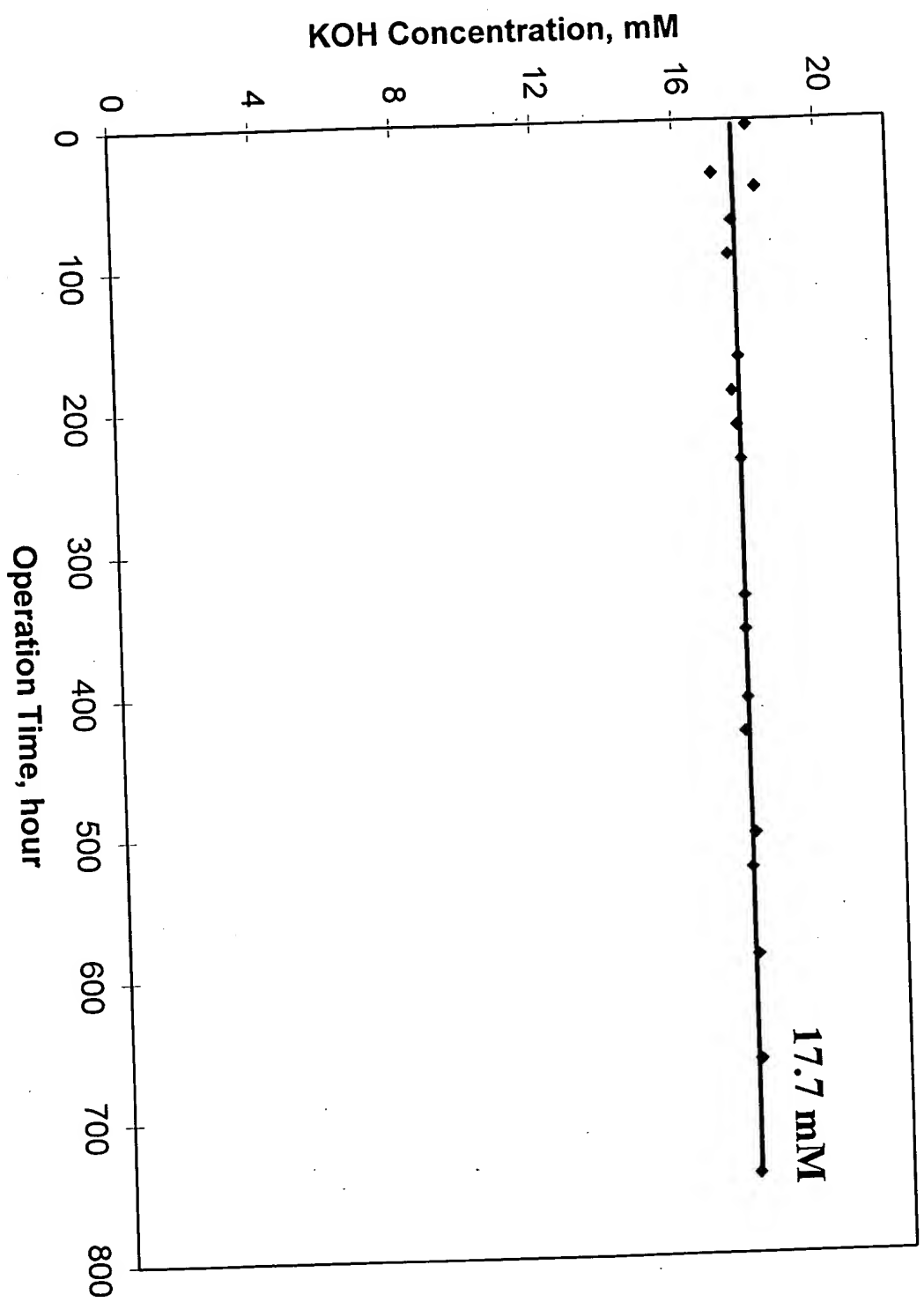


Figure 15.

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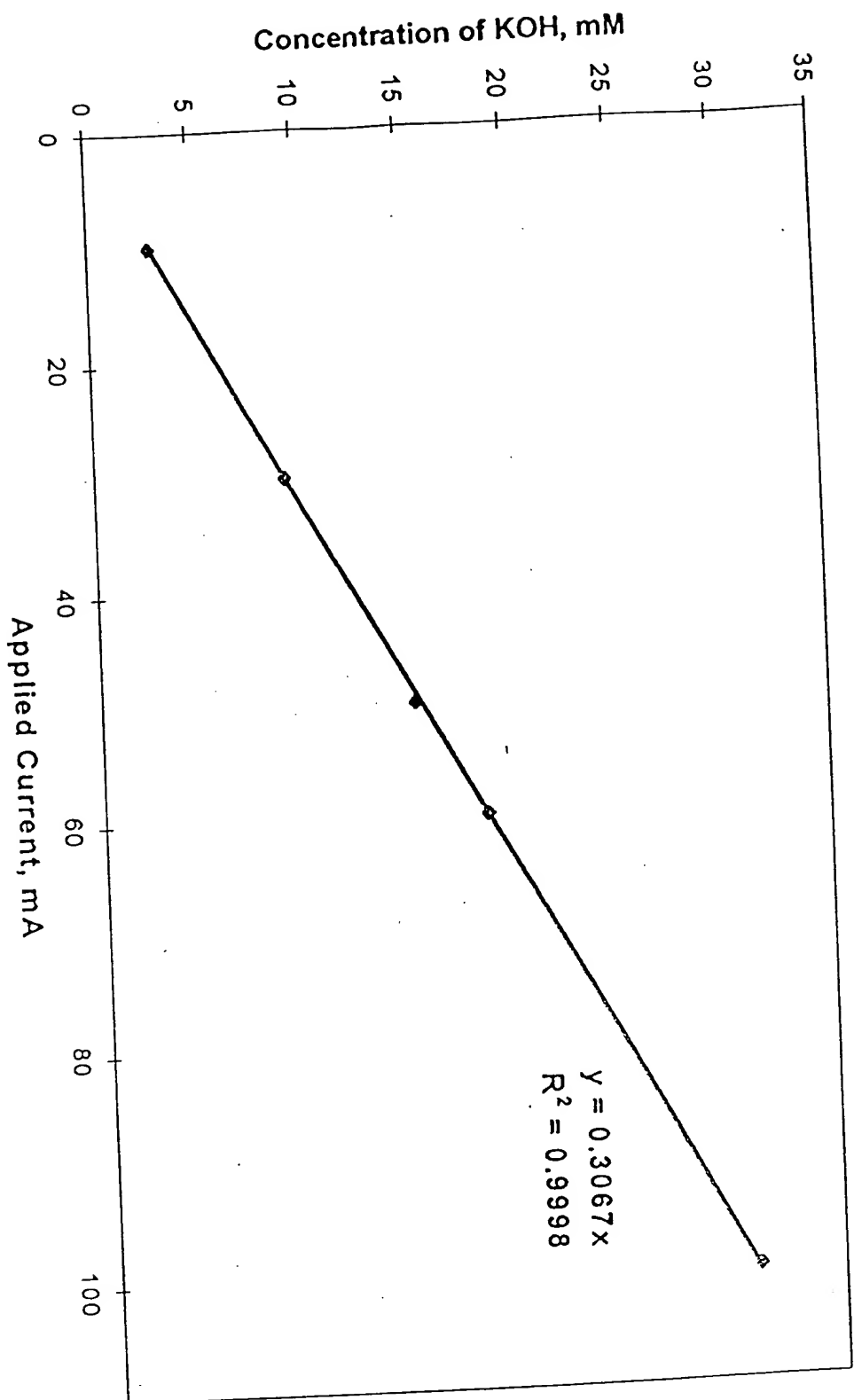


Figure 16

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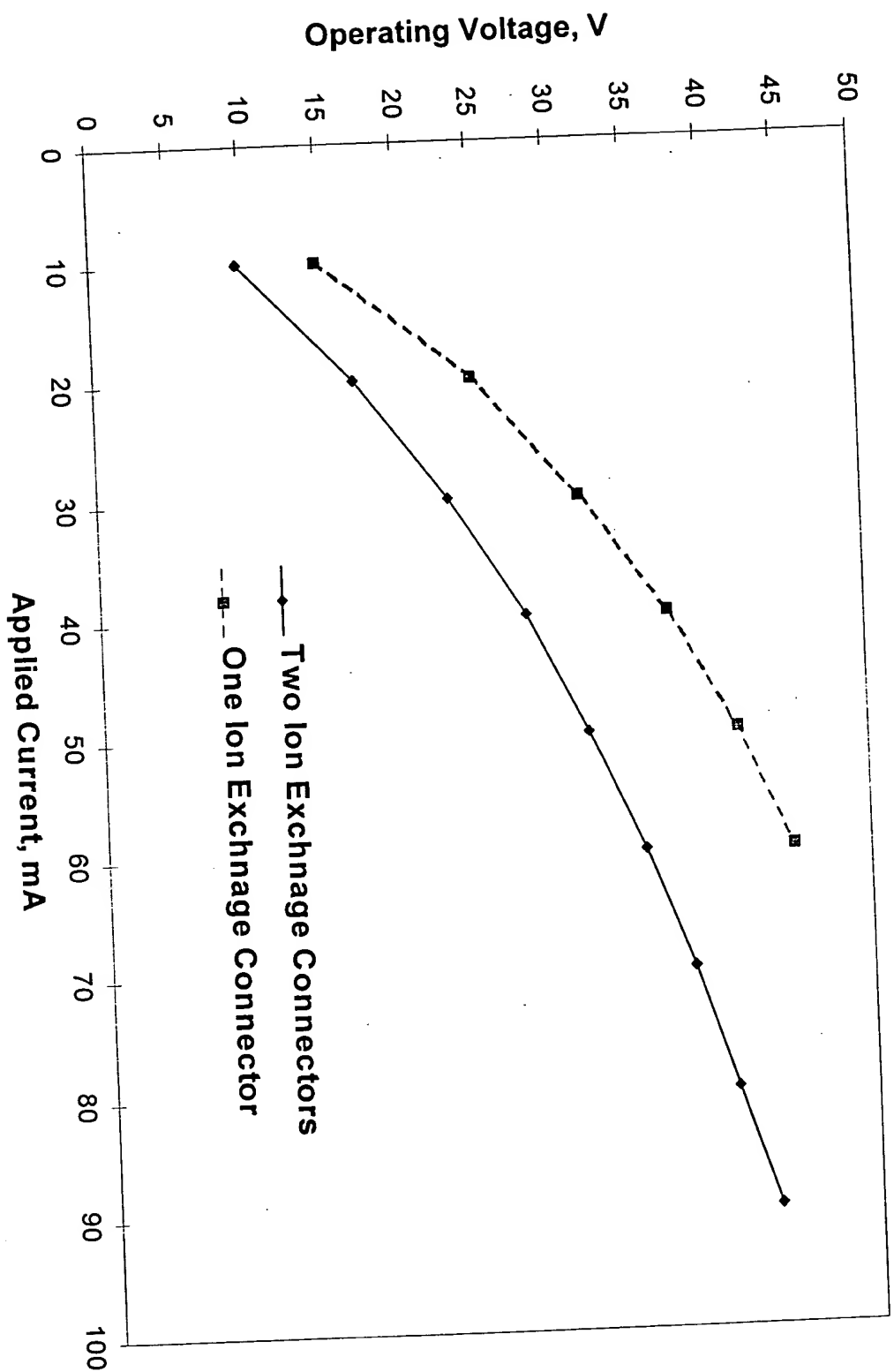


Figure 17

100% of the total current is carried by the two ion exchange connectors.

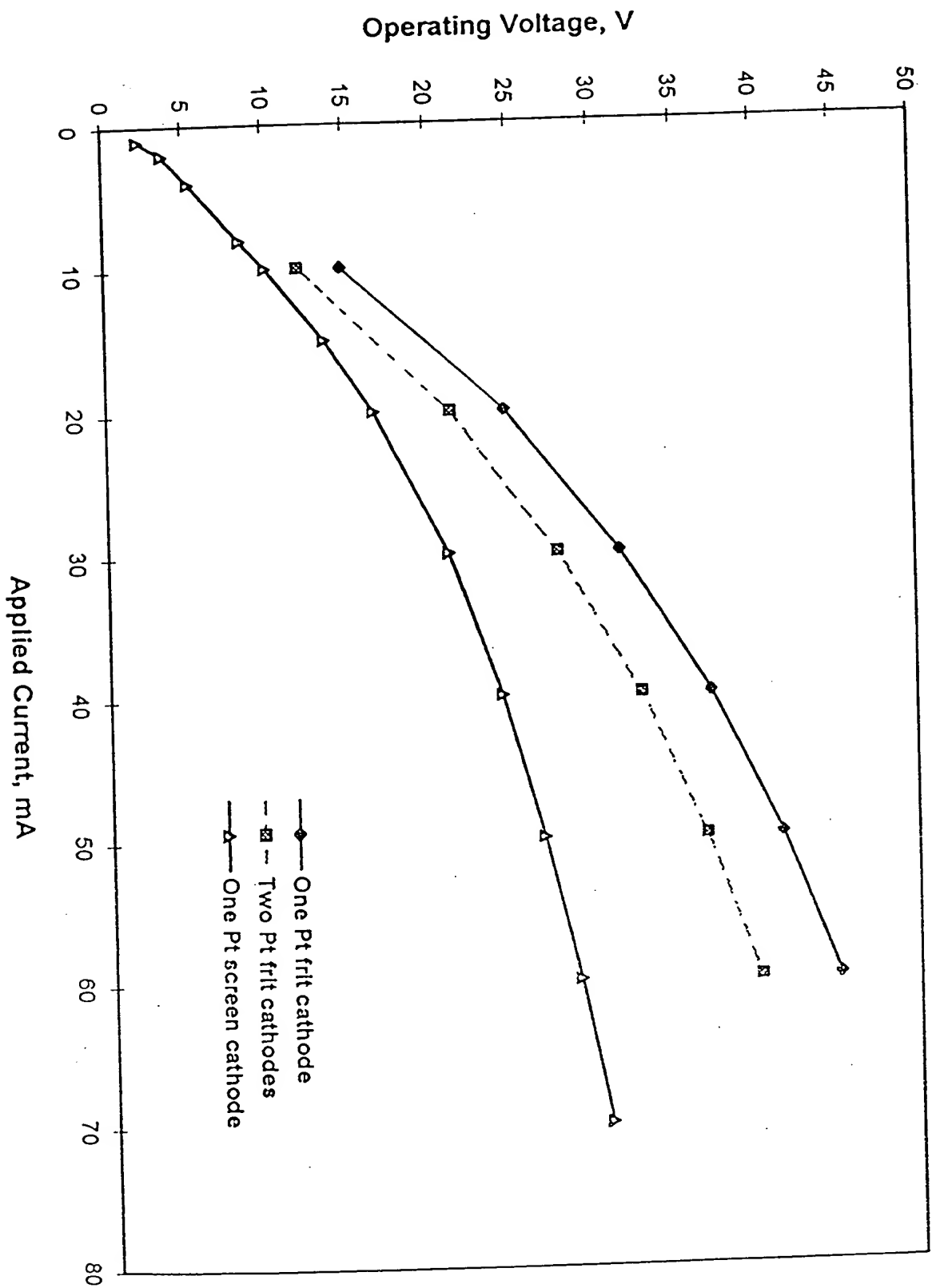
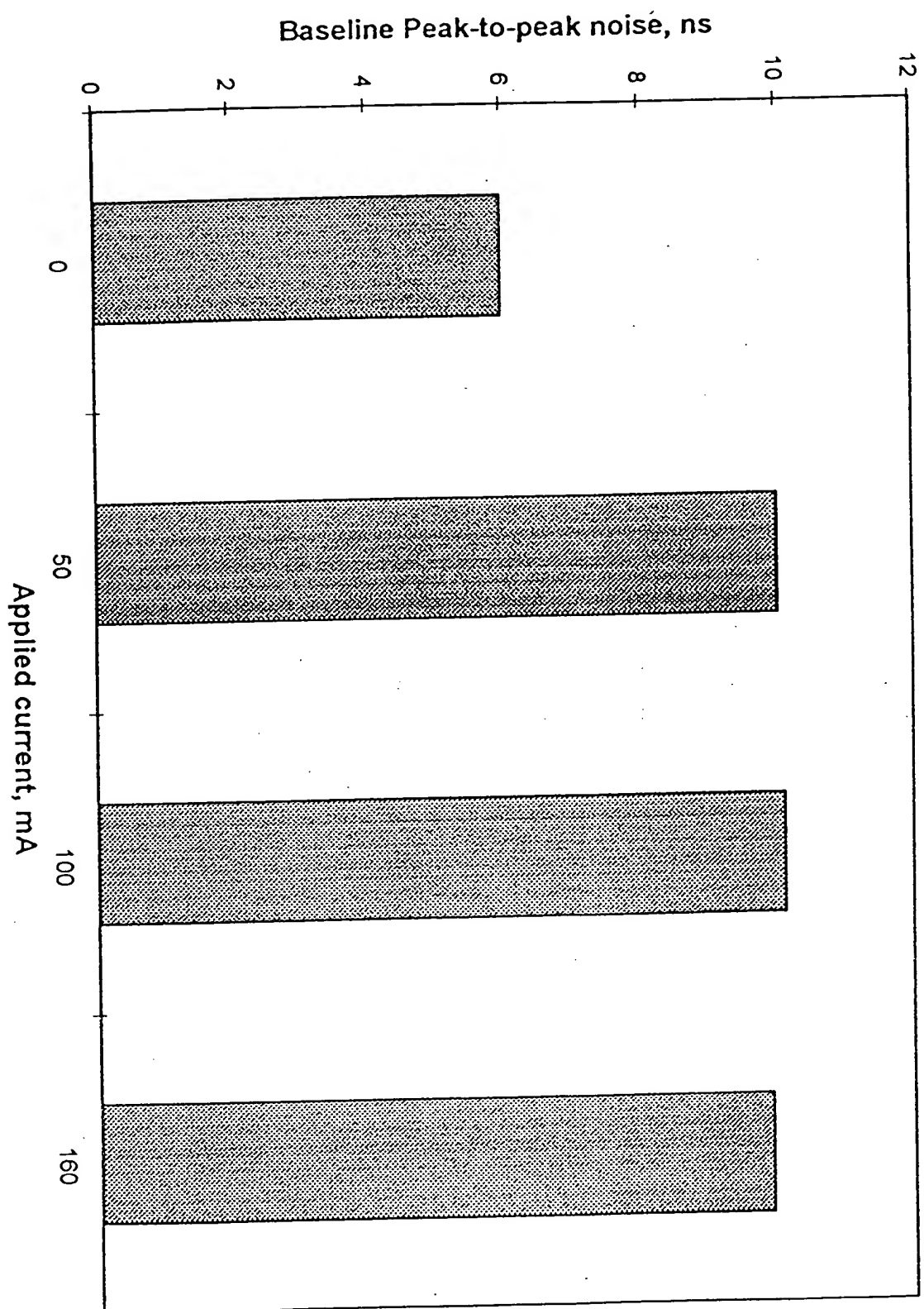


Figure 18

THESE DATA WERE OBTAINED FROM A STUDY OF THE EFFECT OF CATHODE CONFIGURATION ON THE OPERATING VOLTAGE OF A VACUUM TUBE.



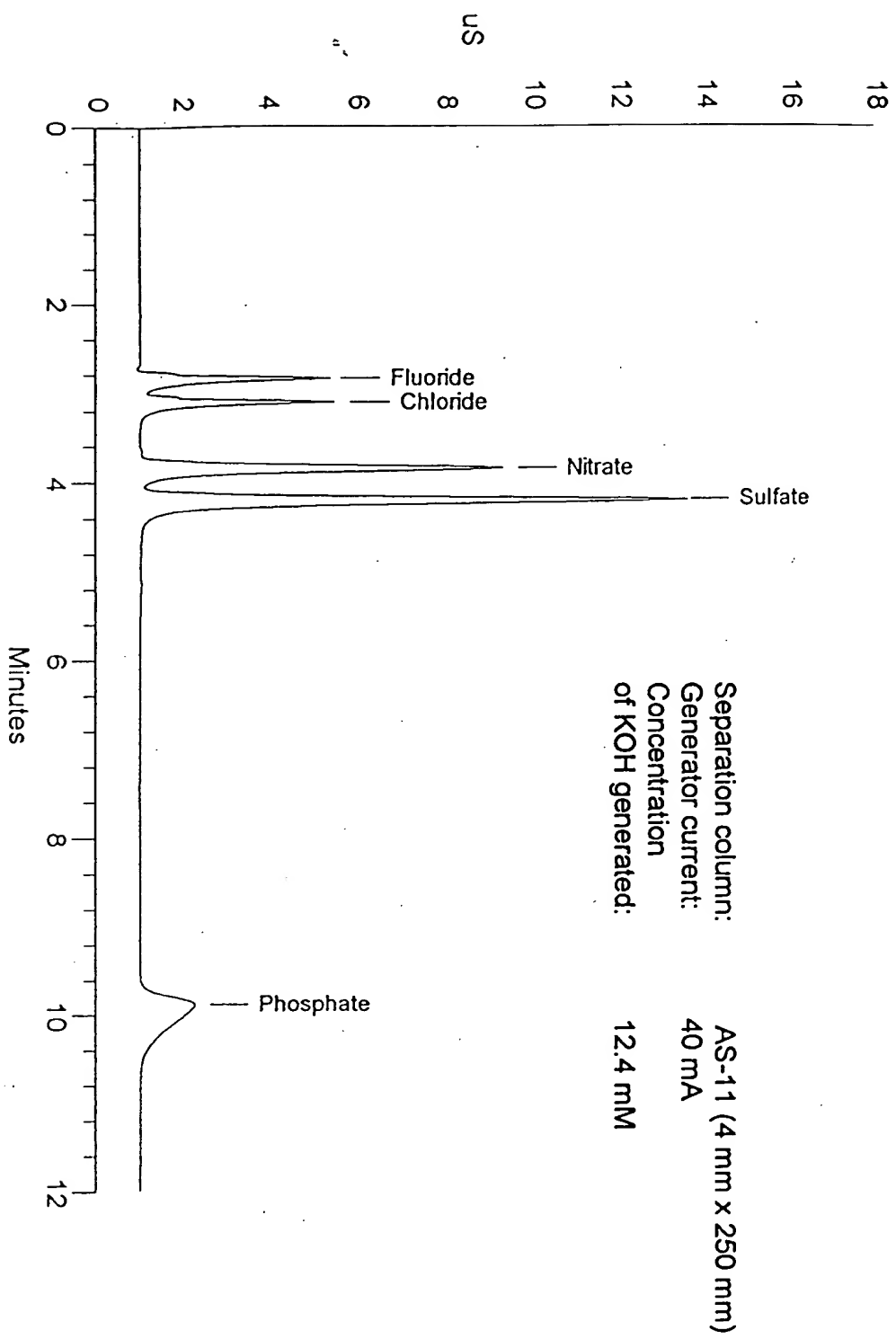


Figure 20.

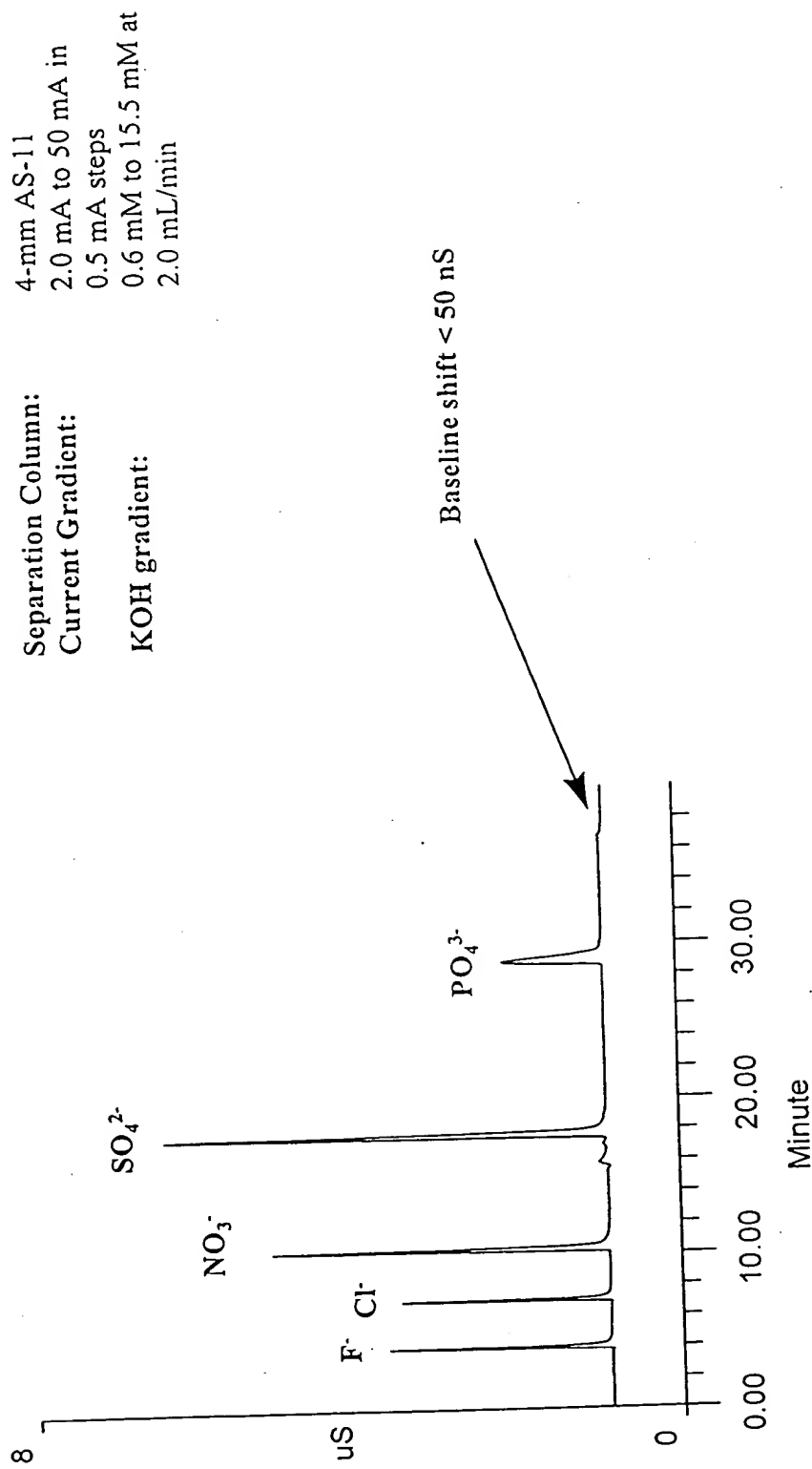


Figure 21.

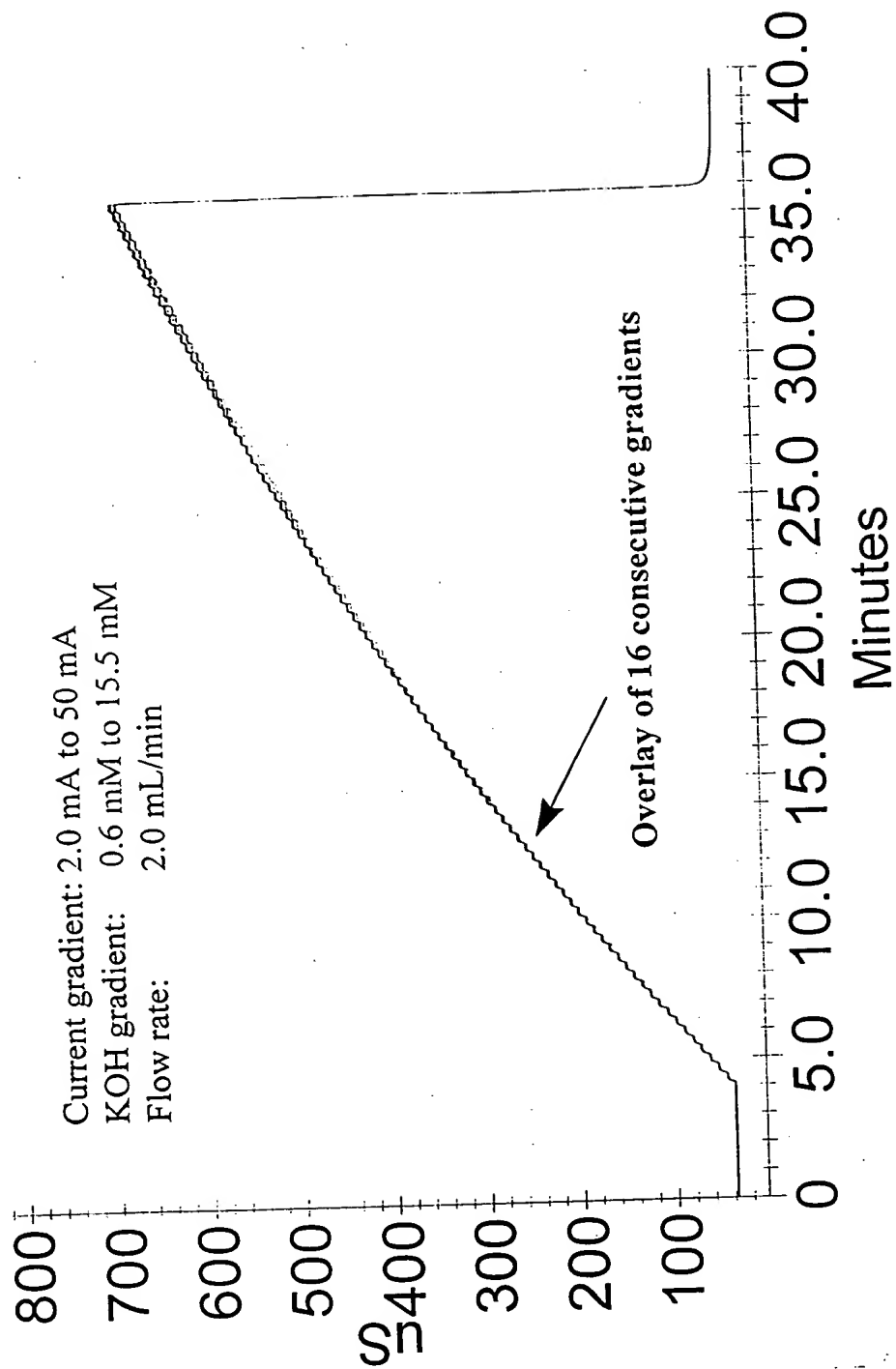


Figure 22.

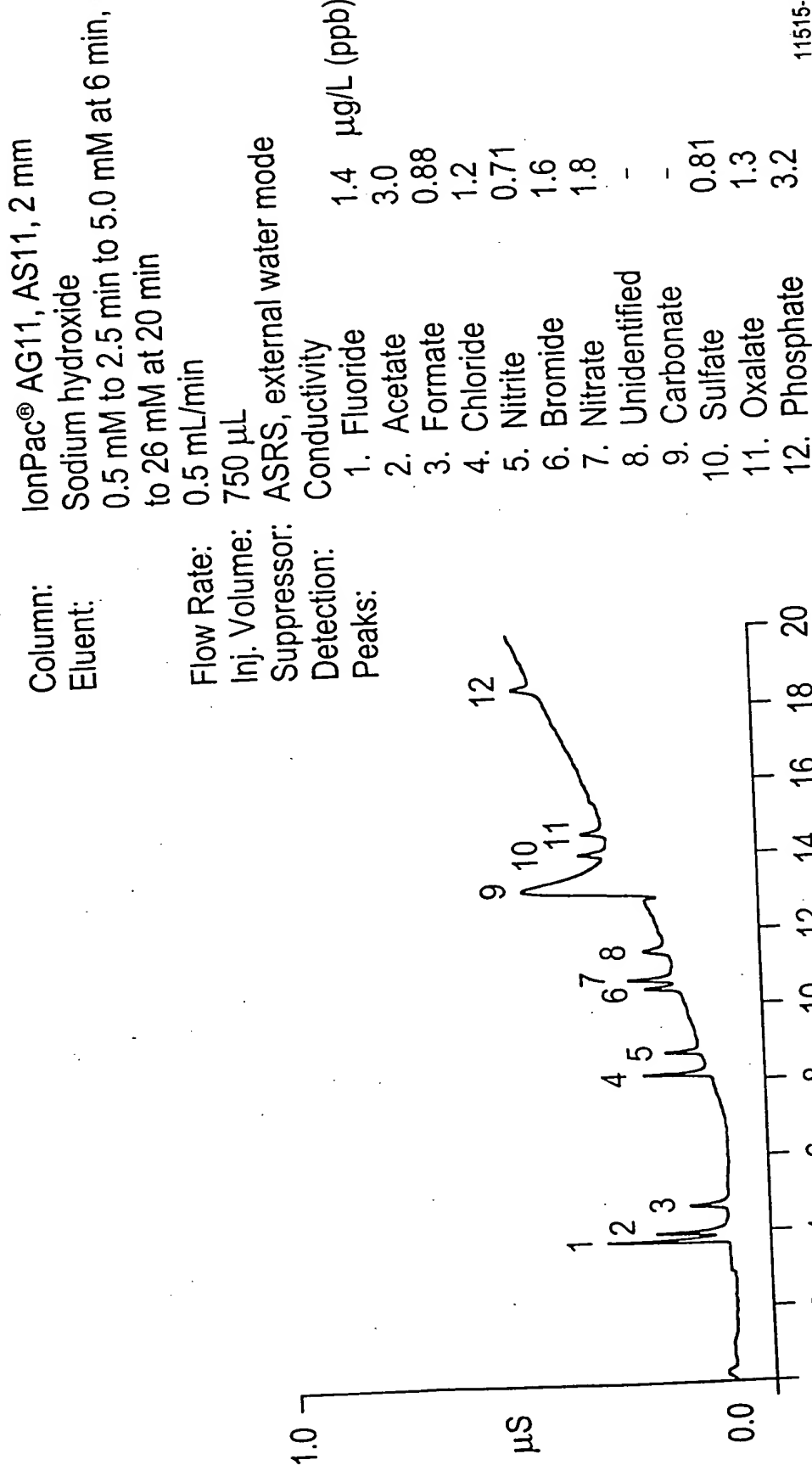


Figure 23.

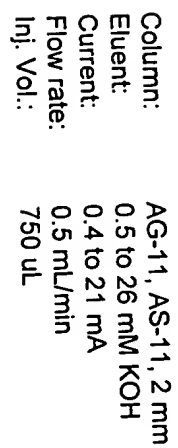


Figure 24.

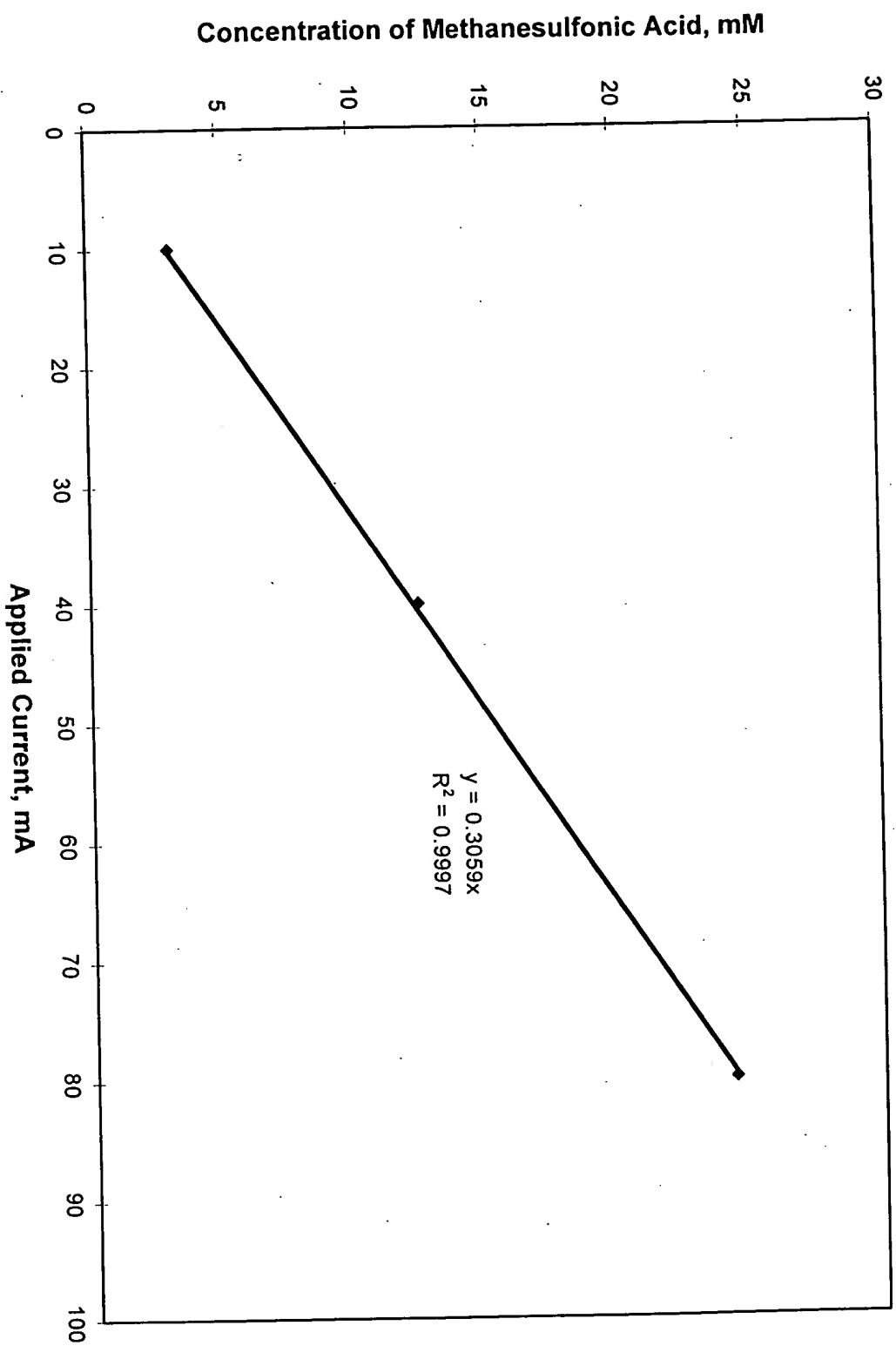


Figure 25.

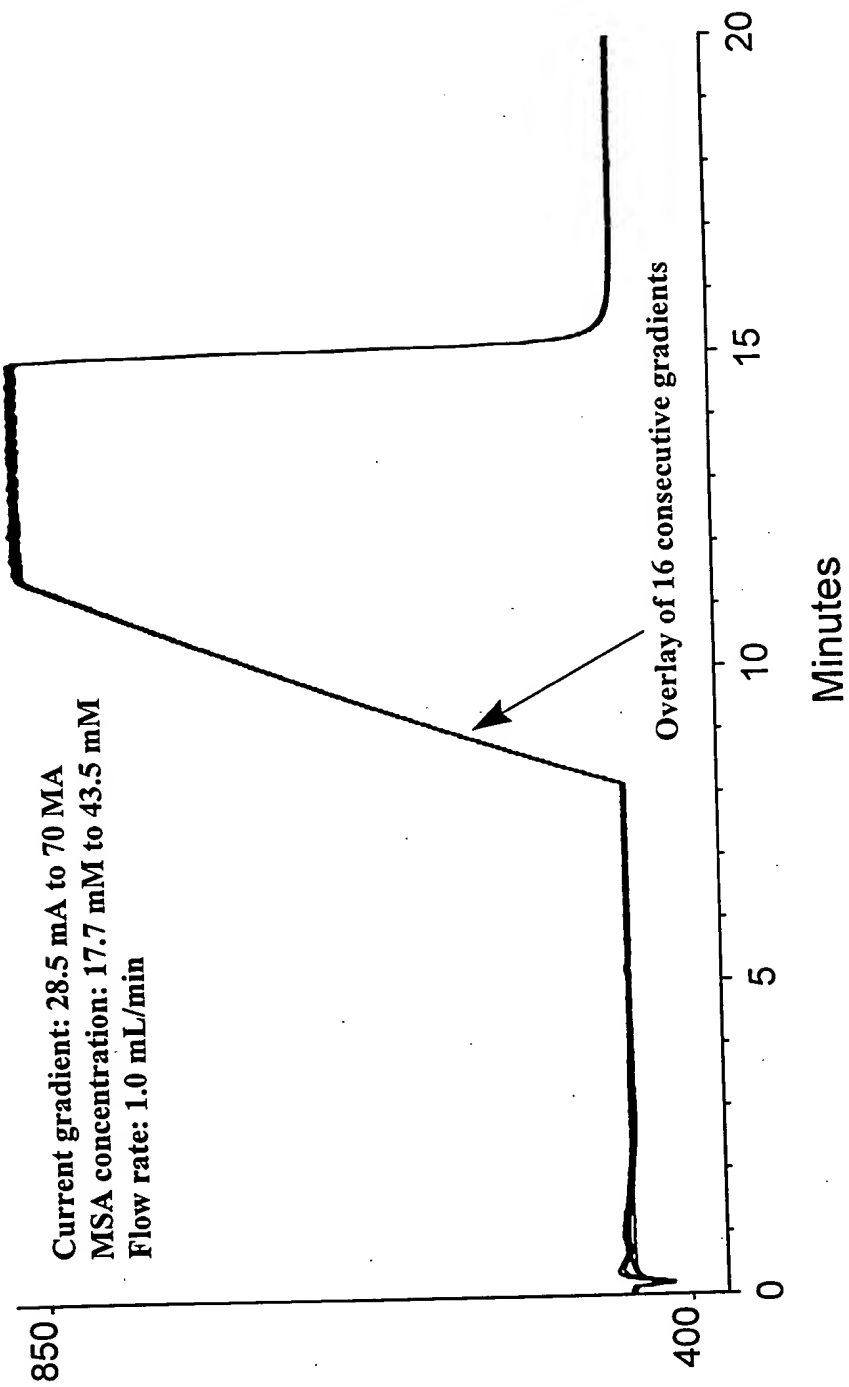


Figure 26

CS12a (4 mm x250 mm)
17.7 mM to 43.5 mM MSA
28.5 mA to 70 mA
1.0 mL/min
750 uL

Column:
Eluent:
Current:
Flow rate:
inj. Volume:

Peak:
1. Lithium 5.0 ppb
2. Sodium 20
3. Ammonium 40
4. Potassium 20
5. Rubidium 100
6. Cesium 100
7. Magnesium 20
8. Calcium 100
9. Strontium 100
10. Barium 150

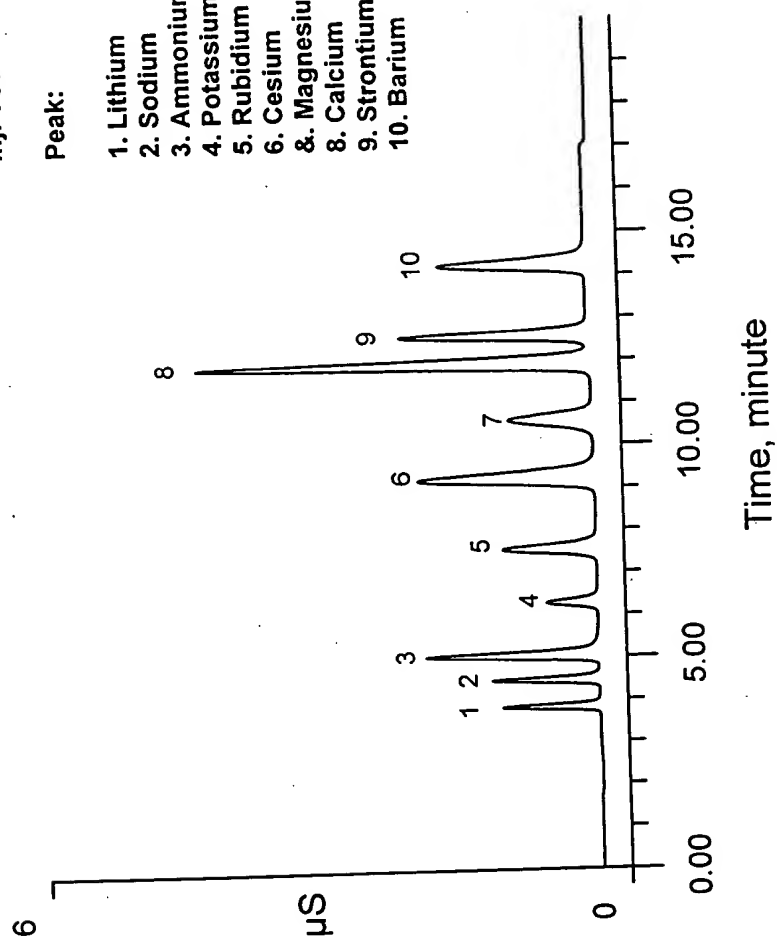


Figure 27.

Column: CS12a
 (4 mm x250 mm)
 Eluent: 17.7 mM
 to 43.5 mM MSA
 Flow rate: 1.0 mL/min
 inj. Voume: 750 uL

- Peak:
- | | |
|--------------|----------|
| 1. Lithium | 0.16 ppb |
| 2. Sodium | 0.63 |
| 3. Ammonium | 1.25 |
| 4. Potassium | 0.63 |
| 5. Rubidium | 3.13 |
| 6. Cesium | 3.13 |
| 8. Magnesium | 0.63 |
| 8. Calcium | 3.13 |
| 9. Strontium | 3.13 |
| 10. Barium | 4.69 |

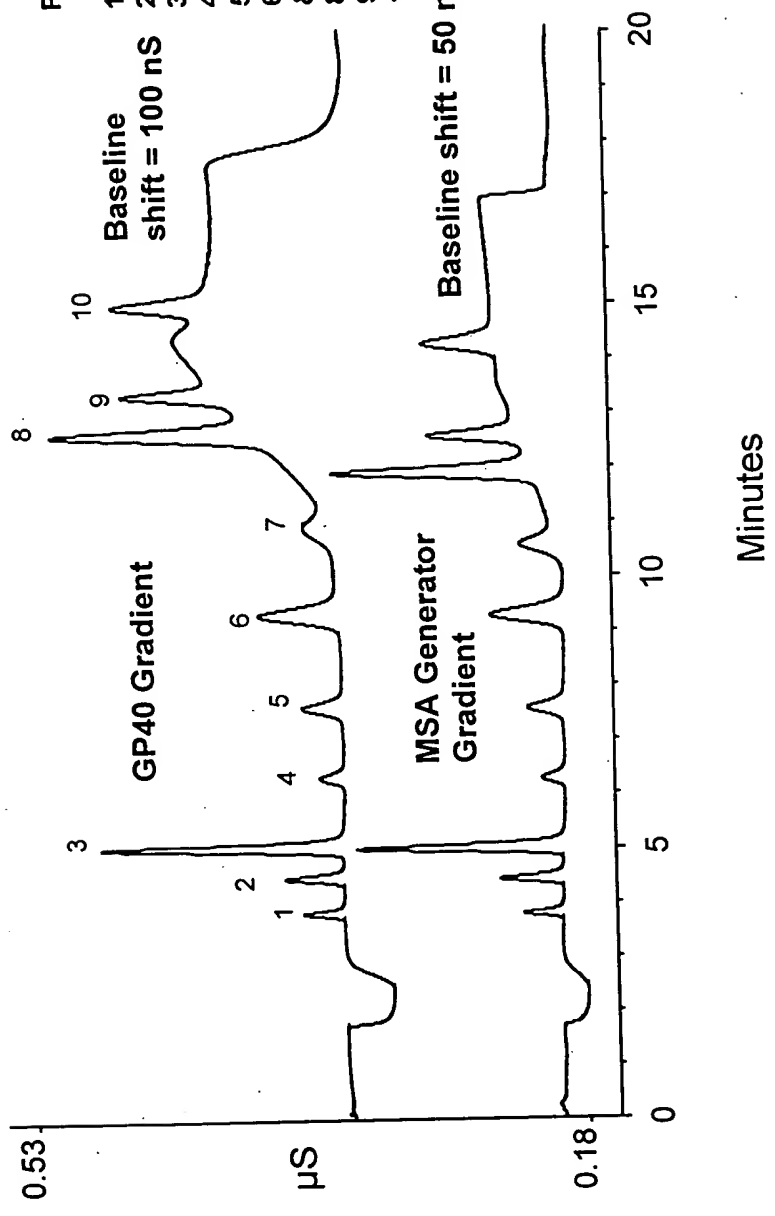


Figure 28.

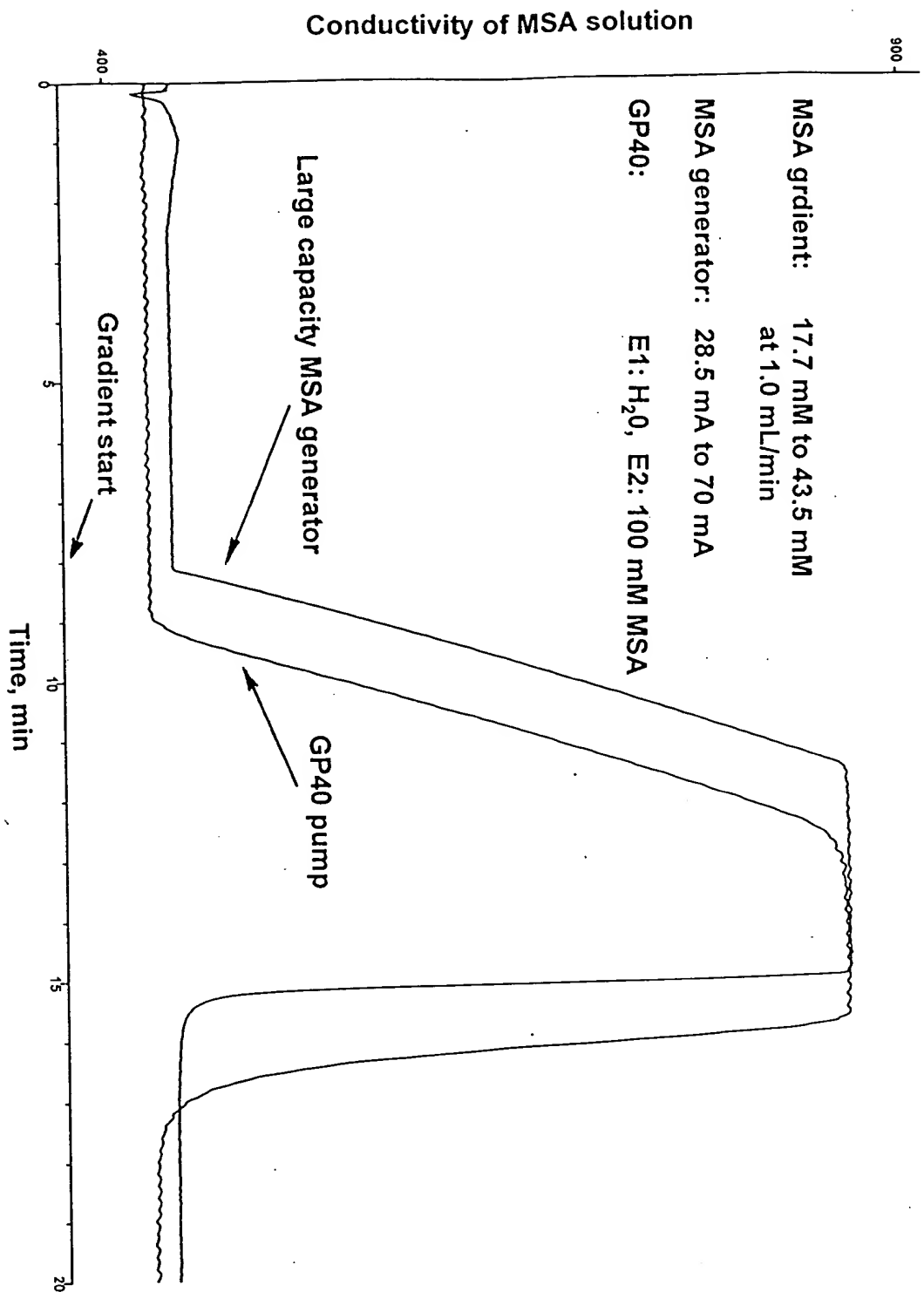


Figure 29.